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### Real Time PID Control of Multiprocess System

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**ABSTRACT:** Process control is one of the significantchallenges in today industries. In many industrial environments tightlevel, temperature, pressure and flow regulation is needed. Increasingly PID controllers are all now broadly accepted in wide range of sectors. Thekeyaim of this study is to examinehow well theconventional PID controller effectively handle diverse process variables which includes level, flow, pressure and temperature. The PID controller's performance is tested through real time SCADA software. The results indicates that the PID control scheme deliver good outcomes for multiple types of parameters.

Keywords: Level Process, Flow process, Pressure Process, Temperature Process, PID controller, SCADA

#### I. INTRODUCTION

The most important part of any control engineering and operational industry is designing a controller and turning it into an automatic control. The purpose of this work is to device a new PID controller for a multi-process (Level, Flow, Pressure, and Temperature). In many processes plant, all of the process variables are vital. In all industrial systems, regulating and holding the Process Parameters at a desired condition (set point) is an important and usual task. The output (process variable) is continuously determined with theaid of a sensing device and manipulated with the help of a controller to hold at a desired target value in closed loop control.Multi Process Control System was established to explore various control loops. Since it is a highly versatile and flexible technology, this may be utilized in wide industrial processes like flow, level, temperature and pressure[1]. Thus, it is basically used for elaborating the study of process parameters relative to flow, level, temperature and pressure. The system is equipped with transducers, actuators, PID and computerized control with DAQ Controller Software [2].

#### **II. DESCRIPTION FOR MULTI PROCESS CONTROL**

Arrangement depicted in Fig 1is developed to assist extensive controlmechanismapplied in variety of industrial operation. This system is composed of multi process control Trainer, pump, hand valves, rotameter and one reservoir tank[3,4]. The pumps are used to draw water from reservoir tanks and distribute it to process tanks and control output of controller. A rotameter is used to monitor the flow rate of intake water to process tanks. The level in a process tank is sensed detects the level in the process tank. The Temperature in the process tank is sensed using a Temperature sensor and the Pressure sensor detects the pressure in the pipeline. The necessary front panel diagram seen in Fig2 has been installed is mounted on hold-alone style of arrangement. This set-up is linked to PCvia COM 3 port with SCADA software for measuring and control of the conventional controller.[5].

Feedback control is a control strategy that manipulates a variable utilising the data from evaluations to get the desired outcome. The parameter being controlled is measured and compared to a target value in feedback control.

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Fig 1 Setup of Multiprocess Trainer

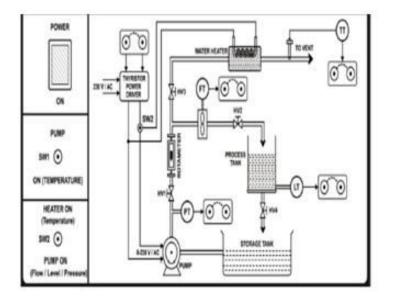


Fig 2 Front panel diagram of Multi ProcessEquipment

#### **III.MULTI PROCESS TRAINER TUNING**

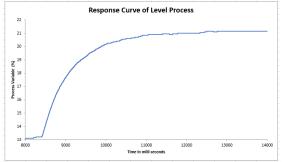
The open loop Process Reaction Curve Method is used to estimate the transfer function of the multi-process system The transfer function and PID controller parameters are obtained using a two-point tuning methodology [13]. The level, flow, Pressure and Temperature process transfer function can be calculated from Fig 3,4,5,6.  $T_2$  and  $T_1$  is 63.2% of final output and 28.3% of finaloutput. Equations (1), (2) and (3) can be utilized to derive theparameters Process gain ( $K_p$ ), dead time ( $t_d$ ), time constant ( $\tau$ ).

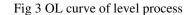
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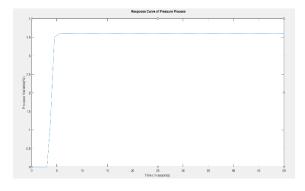


Fig 5 OL curve of pressure process

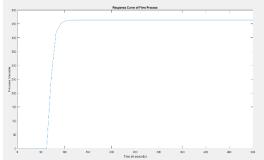


Fig4 OL curve of flow process

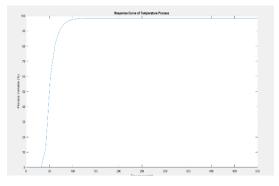


Fig 6OL curve of temperature process

(4)

(6)

$K = \frac{Change\ in\ output}{Change\ in\ input}$	(1)
$\tau = 1.5(t_2 - t_1)$	(2)
$T_d = (t_2 - \tau)$	(3)
The transfer function for level process = $\frac{1.63 e^{-13.9s}}{1.22s+1}$	(4)

The transfer function for flow process = 
$$\frac{1.16 \ e^{-65.04s}}{6.91s+1}$$
 (5)

The transfer function for Pressure process = 
$$\frac{1.2 e^{-2.55s}}{0.26s+1}$$

The transfer function for temperature process = 
$$\frac{1.64 e^{-39.6s}}{12.5s+1}$$
 (7)

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Process	K <sub>P</sub>	Ki	K <sub>d</sub>
Level	0.048	46.28	0.00103
Flow	0.082	216.58	0.0038
Pressure	0.078	8.505	0.0090
Temperature	0.174	131.88	0.0001

#### Intended Variables of PID Controller

#### IV. ASSESSMENT TECHNIQUE& HARDWARE PARTICULARS

The PID controlmechanism is carry out to explore how to keep the level, flow, Pressure and temperature at the right number. The PID controller more accurately fix the set point values. The featuresoffered in the PID controller accessible by Supervisory Control and Data Acquisition (SCADA) software are shown in Fig.7 & 8. Fig 9 shows the screen shot of values while the process is running.

Group Details			> Process						×
Process Group			Proc						
Group No:	0			Process No: Group No:	3 0				
Group Name:	DTC			cess Name:	LEVEL				
Controller Name:	DTCSeries	~	Pro	cess Type:	Single Loop V				
Serial Port Setup			PID						
Serial Port :	COM3	•		tation Address: V and SV	1	Internal Details			
Baud Rate :	9600	~		PV Name	e: PV	🕑 Enable Logg	ng / Visible		
Parity :	Even	$\sim$		SV Name		🔄 Enable Logg	ng / Visible		
Data Bits :	8	~		Uni					
Stop Bits :	1	$\sim$				•			
Flow Control :	None	~			CV	Enable Loog	ng / Visible		
Interval :	100	mSec			an ear				
Timeout :	200	mSec			• 2				
DTC Dataila									~
DIC Details									^
Input Det	ails								
Input	Type:	4~20mA	~	De	cimal Place:	0.0	$\sim$		
Low	Count	0		Sc	ale Min:	0			
High	pp Bits : 1 Control : None terval : 100 mSec imeout : 200 mSec OK Cancel OK Cancel OK Cancel OK Cancel A Concel OK Cancel OK Cancel OK Cancel OK Cancel OK Cancel OK Cancel								
Output-1	Details				Output-2 Det	ails			
Contr	rol Type:	Heating	~		Control 1	Type: Alam	n	~	
							ж	Cancel	

Fig 7 Properties available with SCADA software

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⇒ FL	_			
Sta	art Logging Stop Logging PID Logging Hist	Logging To C:\\FLOW23_Mar_2011_12_14_56.jts		
V	225.0 LPH	150.0 CV LPH 36.	0 %	
	Time(1x100 mSec)	PV(LPH)	SV(LPH)	CV(%)
	2625	225.0	150.0	36.0
_	Time(1x100 mSec)	PV(LPH)	SV(LPH)	CV(%)
	2311	223.0	150.0	36.0
	2312	223.0	150.0	36.0
	2313	223.0	150.0	36.0
	2314	223.0	150.0	36.0
	2315	223.0	150.0	36.0
	2316	223.0	150.0	36.0
	2317	223.0	150.0	36.0
	2318	223.0	150.0	36.0
	2319	223.0	150.0	36.0
	2320	223.0	150.0	36.0
	2321	223.0	150.0	36.0
	2322	224.0	150.0	36.0
	2323	224.0	150.0	36.0
	2324	224.0	150.0	36.0
	2325	224.0	150.0	36.0

Fig 8 Screen Shot of Values while Process is running

Table 1 Level Transmitter Characterization

Input Voltage	24 Volt DC
Output scaling	4 to20 mA
Range	0 to25 cm
Туре	RF Capacitance

Table 3: Pressure Transmitter Characterization

Input Voltage	24 Volt DC
Output scaling	4 to20 mA
Range	0 to 5bar / (0-1000) mmwc
Туре	RF Capacitance

Input Voltage	24 Volt DC
Output scaling	4 to20 mA
Range	0 to 100
Туре	RTD (PT 100)

Table 4: Temperature Transmitter Characterization

Table 2 Flow Transmitter Characterization

24 Volt DC

4 to20 mA

(0-500) LPH Turbine

Input Voltage

Output scaling

Range

Type

#### V. REAL TIME RESULTS AND DISCUSSIONS

The responses of Individual processes including level, flow, pressure, and the temperature process system deliver good outcomes. To authenticate the steady Proportional-Integral-Derivative controller, a real time test was done on level, flow, pressure, and temperatureprocess. We assessed the set point of 15 cm for level process, 350 LPH for flow, 2.5 bar for pressure and 3deg for temperature and the plot is shown in fig 9a,9b,9c, &9d. The controller has produced good settling for all the process. In future the transfer function may be put up in MATLAB Simulink software using various controllers and the performance can be evaluated.

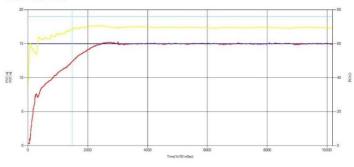


Fig 9a Response for level with SV=15 CM

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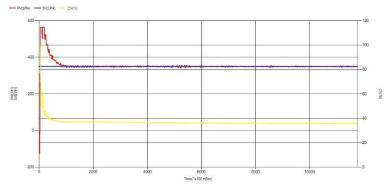


Fig 9b Response for flow with SV= 350 LPH

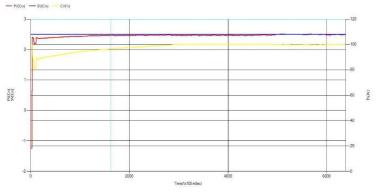


Fig 9cActual Response for Pressure with SV=2.5 bar

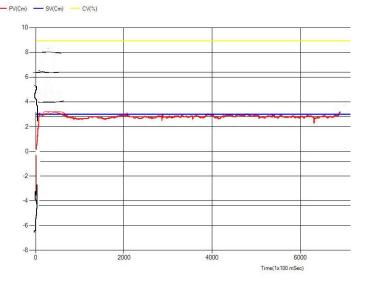


Fig 9d Actual Response for Temperature with SV= 3 deg

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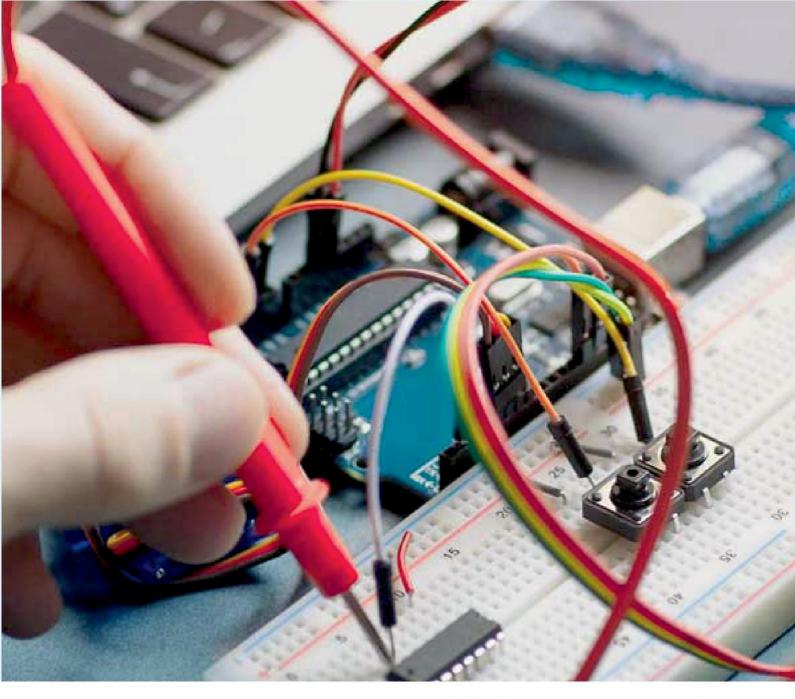


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#### REFERENCES

- [1] Real time Design of PID Controller for Process control system Urvashi Pande Yogesh V. Hote 2020
- [2] Simulation of Cascade Control for aMultiprocess Station using Fuzzy Logic 2015
- [3] F. Haugen and B. Lie, "Relaxed Ziegler-Nichols closed loop tuning of PI Controllers," Modeling, Identification and Control, vol. 34, no. 2, pp. 83-97, 2013
- [4] Julio Ariel Romero, Roberto Sanchis, Pedro Balaguer," PI and PID auto-tuning procedure based on simplified single parameter optimization", journal of process control 21 (2011) 840–851.
- [5] Stuart A. Boyer, SCADA: supervisory control and data acquisition, International Society of Automation: 2009
- [6] Adnan Salihbegovica, Vlatko Marinkovica, ZoranCicoa, ElvedinKaravdicb and Nina Delica, "Web based multilayered distributed SCADA/HMI system in refinery application" Computer Standards & Interfaces, vol. 31, p. 599-612, March 2009
- [7] Vinay M. Igure, Sean A. Laughtera, and Ronald D. Williamsa, "Security issues in SCADA networks" Computers & Security, vol. 25, p. 498- 506, October 2006
- [8] David Bailey and Edwin Wright, "2 SCADA systems, hardware and firmware" in Practical SCADA for Industr: 2003, 11-63
- [9] S.H Yang, X Chena, and J.L Altya, "Design issues and implementation of internet-based process control systems", Control Engineering Practice, vol. 11, p. 709-720, June 2003
- [10] S. Stefani and H. Savant, Design of feedback control systems, 4thedn. Oxford University Press, 2002.
- [11] Jing-Chung Shen," New Tuning Method for PID Controller",Proceedings of the 2001 IEEE International Conference on ControlApplications, September 5-7, 2001 Mexico City, Mexico.
- [12] J. G. Ziegler and N. B. Nichols, "Optimal settings for automatic controllers," Trans. ASME, vol. 64, pp. 759-768, 1942
- [13] B.WayneBequette, Process control Modeling, Design and Simulation (Prentice Hall, USA, 2003).





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